1. Introduction

Carbon dioxide emission in the atmosphere is an increasingly important concern, owing to its perceived influence on the elevation of atmospheric temperature. Of the various approaches discussed to limit this threat, selective carbon dioxide capture by absorption followed by its sequestration is one of the most scrutinized strategies. Several research efforts are ongoing to design and develop new sorbents for selective CO₂ capture from power plant flue gases as well as other CO₂ discharging streams. The development of advanced functional materials satisfying the essential requirements of faster sorption kinetics, higher sorption capacity, selectivity and durability is therefore of great significance.

Currently, there is significant interest in the development of regenerable sorbent materials for CO₂ absorption at high temperature. Among the various carbon dioxide sorbents, lithium-based ceramic absorbents are candidate materials for CO₂ capture at high temperatures (400–700 °C). In particular, lithium orthosilicate is considered to be the most promising material for designing efficient CO₂ separation systems by virtue of its large absorption capacity, faster kinetics and reasonable material costs. Moreover, lithium silicate shows excellent chemisorption properties, absorbing up to 8.3 mmol of CO₂ per gram of sorbent. It also exhibits better thermal cyclability over a wide range of temperature.

A number of strategies are reported in the literature for the synthesis of Li₄SiO₄, which include solid-state mixing, sol–gel synthesis, combustion synthesis and ball milling techniques. The original inventors of lithium-based CO₂ absorbents, investigated CO₂ absorption properties of Li₄SiO₄ and Li₂ZrO₃ in a wide range of temperature and CO₂ concentrations. Their results showed that under similar sorption conditions, the absorption capacity of Li₄SiO₄ is 30 times greater than that of Li₂ZrO₃. Lithium silicate is commonly synthesised by the reaction between silica and lithium carbonate powders under dry or wet conditions in a ball mill, followed by heat treatment. Such solid-state mixing processes are known to result in poor distribution of powder particles, leading to inferior absorption properties. Numerous other issues such as contamination, volatilization as well as agglomeration of particles, leading to inconsistency in structure and composition, are also reported. Wet chemical approaches are known to produce materials with controlled particle sizes, uniform size distribution, excellent homogeneity and large surface area. Such desirable powder attributes help to realize high sorption capacity and faster kinetics in absorbent materials. Our group was one of the first to report on the sol–gel
synthesis of lithium zirconate-based absorbents for the selective removal of CO₂.\textsuperscript{18,24} Pfeiffer \textit{et al.} have compared the influence of processing conditions, such as solid-state reaction, precipitation and sol–gel method on the composition and morphology of lithium metasilicate powders meant for breeder material applications.\textsuperscript{19} The same authors have also reported on the wet chemical synthesis of lithium silicate-based absorbents in their recent papers.\textsuperscript{26,40} The effect of particle size of the precursor materials on the mixing of the precursors is reported recently by Lu \textit{et al.}.\textsuperscript{25} Peng \textit{et al.} have reported the effect of precursor silicon source (diatomite and pure silica) on carbon dioxide absorption capacities of the resulting powders and have shown that Li₄SiO₄-based sorbents developed from diatomite exhibited better absorption–desorption performance and absorption capacity.\textsuperscript{41} Results discussed in the said papers point to the importance of precursor chemistry, their physical properties, and the processing conditions on the CO₂ absorption performance of the resulting materials.

The present work reports on the synthesis of Li₄SiO₄ platelet-shaped particles by a wet chemical synthetic procedure involving colloidal silica and LiNO₃ solutions. The sorption/desorption kinetics of CO₂ and the cyclic stability of the synthesised particles are reported. The excellent CO₂ absorption performance exhibited by supported lithium silicate absorbents, coated on a porous carbon strip, is also reported in this paper for the first time, to the best of our knowledge.

2. Experimental section

Lithium silicate was synthesised from lithium nitrate (Alfa Aesar, UK) and colloidal silica (Aldrich Chemicals, USA) as starting precursors. Initially, 15.4 g of LiNO₃ was dissolved in 225 ml of distilled water to prepare 1 M aqueous lithium nitrate solution and was hydrolysed by the slow addition of ammonium hydroxide solution (25\%, S.D. FINE-CHEM Ltd., India) under constant stirring at room temperature, until the pH reached 8. Then, 3.3 g of colloidal silica (Aldrich Chemicals, USA) was added dropwise to this reaction mixture with constant stirring, and the resulting solution was stirred for 1 h. The gel thus formed was aged further for 24 h at room temperature, dried at 110 °C and then heat-treated at 800 °C (sample code: SG-LiSiO₄). Samples for comparison were prepared by the solid-state mixing and heat-treatment of silica and Li₂CO₃ (Aldrich Chemicals, USA). Both the precursors were initially dried at 150 °C for 5 h and mixed mechanically in the molar ratio of 2.2 : 1. The mixture was dried at 100 °C for 6 h and calcined at 800 °C for 3 h (sample code: SS-LiSiO₄). The crystalline phases of the powdered samples were analysed by X-ray diffraction (Philips XPert Pro diffractometer) in the 2θ range 20–60° using Cu Kα radiation (λ = 0.154 nm). The morphological and microstructural analyses of the materials were carried out using a scanning electron microscope (SEM) operated at 20 kV. The BET surface area measurements were carried out by nitrogen adsorption using a Micromeritics Gemini 2375 surface area analyzer after degassing each sample at 200 °C for 2 h. CO₂ absorption properties were measured using a TGA apparatus (Perkin-Elmer STA 6000, Netherlands), in the temperature range of 150–750 °C. In the set up used, actual temperatures close to sample were typically 5–10 °C lower than the set temperatures that are mentioned throughout this paper. CO₂/nitrogen flow rates through the sample chamber were ~50 ml min \(^{-1}\) unless otherwise mentioned. X-ray scattering set-up (Xeuss SAXS/WAXS system by Xenocs, France) was used to characterize the sample after CO₂ absorption using Cu Kα radiation (λ = 0.154 nm) generated at 0.60 mA and 50 kV in the 2θ range 4–36°.

3. Results and discussion

The CO₂ absorption mechanism of lithium orthosilicate involves the chemical conversion of lithium orthosilicate to lithium metasilicate or silica by the reaction with CO₂ as in the following equations.\textsuperscript{20}

\[
\text{Li}_4\text{SiO}_4 + \text{CO}_2 \rightarrow \text{Li}_2\text{SiO}_3 + \text{Li}_2\text{CO}_3 \\
\text{Li}_2\text{SiO}_3 + \text{CO}_2 \rightarrow \text{Li}_2\text{CO}_3 + \text{SiO}_2
\]

Based on reaction (1), the theoretical absorption capacity of the Li₄SiO₄ solid absorbent (MW = 119.854) could be calculated as 36.7 wt% (8.3 mmol of CO₂ per gram of Li₄SiO₄). In practice, 30–35 wt% of CO₂ could be absorbed at the temperature range of 400–700 °C followed by complete desorption at 600–800 °C, depending upon the CO₂ partial pressure, the exact stoichiometry and second phase/impurity present in the absorbent material.\textsuperscript{29} Lithium-rich phases such as lithium orthosilicate and oxosilicate generally display fast kinetics for CO₂ absorption due to the extremely fast lithium ion hopping from the core of the particle to the reaction interface. The completion of the reaction forming silica as per eqn (2) needs absorption conditions favouring the take-up of CO₂ by the lithium metasilicate formed at the initial phase of the reaction and is not typical of the absorption processes reported in literature.

It is reported that, for the wet chemical synthesis of lithium silicate, the preferred precursor is lithium nitrate for reasons that are yet to be fully understood.\textsuperscript{26} Lithium nitrate solution, when hydrolysed, forms lithium hydroxide which undergoes polycondensation reactions with silica, leading to the formation of a gel network.

This wet chemical synthesis reaction leading to the formation of lithium orthosilicate should be as follows:

\[
\text{LiNO}_3 + \text{NH}_2\text{OH} \rightarrow \text{LiOH} + \text{NH}_4\text{NO}_3
\]

\[
4\text{LiOH} + \text{SiO}_2 \rightarrow \text{Li}_4\text{SiO}_4 + 2\text{H}_2\text{O}
\]

The solid-state reaction between lithium carbonate and silica should be as follows:

\[
2\text{Li}_2\text{CO}_3 + \text{SiO}_2 \rightarrow \text{Li}_2\text{SiO}_4 + 2\text{CO}_2
\]
3.1. Phase characterization and morphological studies of Li$_4$SiO$_4$

The X-ray diffraction pattern of the SG-Li$_4$SiO$_4$ powders synthesised through the sol–gel route is shown in Fig. 1(a). The peak data confirmed the formation of Li$_4$SiO$_4$ crystalline phase (JCPDS 37-1472) along with trace amounts of Li$_2$SiO$_3$ phase (JCPDS 29-0828). The formation of the Li$_4$SiO$_4$ phase should be due to the reaction between SG-Li$_4$SiO$_4$ and CO$_2$ from air.\(^7\) Peaks corresponding to unreacted phases of lithium or silica were not observed, and therefore it is safe to assume that the chemical reaction leading to the formation of lithium orthosilicate was complete under the synthesis conditions. The molar composition of Li : Si in the sample was determined to be 4.12 : 1 by chemical analysis. The amount of lithium in the sample is slightly higher than the stoichiometric value of 4 : 1 for Li$_4$SiO$_4$ but remains well within in the range of values normally observed in these ceramics, where excess lithium is added to usually balance any evaporation loss during use.

XRD pattern of the SS-LiSiO$_4$ sample synthesised through the solid-state mixing method as shown in Fig. 1b also had all predominant peaks of lithium orthosilicate (JCPDS 37-1472). The crystallinity of the two samples seems to have some differences, as indicated by the differences in heights of the peaks corresponding to [110] and [011] planes.

Morphological features of the powders were observed in SEM and are shown in Fig. 2. SG-Li$_4$SiO$_4$ appeared to have platelet morphology with length extending more than a micron and width of ~300 nm. Powders made by the solid-state method were found to contain agglomerates with sizes larger than 10 microns and had a non-uniform particle size distribution.

The TEM pictures of the samples as shown in Fig. 3 clearly establish the identity of the constituent structures of the two types of powders. SS-Li$_4$SiO$_4$ particles were observed as hard agglomerates with a size of around 1 micrometer, whereas the SG-Li$_4$SiO$_4$ particle seems to be an assembly of rod-like particles leading to platelet morphology.

3.2. CO$_2$ absorption studies

Fig. 4 represents the dynamic thermograms of the samples measured at 20 °C min\(^{-1}\) using 100% CO$_2$. Three different absorption steps were noticed. The absorption rate was found to be very small up to ~500 °C. The increase in weight at such low temperatures could be attributed to the presence of absorption by lithium metasilicate, which could be present in very small quantities, as evidenced by the XRD results. Lithium orthosilicate is also known to absorb CO$_2$ slightly at this temperature range.\(^7\) A sudden weight increase occurred after this temperature and was followed by a third step extending up to the end, with more or less the same rate of weight increment. It is reported that the CO$_2$ absorption process is limited to the surface initially, and only a superficial reaction occurs, leading to the formation of an external lithium carbonate shell over the surface of the ceramic particles at this step. When the temperature is increased appropriately, the shell is softened, and the reaction extends to the bulk of the material. The second step should be due to the sudden formation of the shell of lithium carbonate around the particles, and the third and final step should be determined by the diffusion of CO$_2$ through the shell and Li$^+$ through the skeleton, thus extending the reaction to the bulk of the material. The second step was less obvious in the solid-state sample, probably because of the lower surface area of the powder. As shown clearly in Fig. 4, the kinetics of absorption was entirely different between the samples; sol–gel samples had a higher absorption capacity at any given time compared to the solid-state samples. At T > 720 °C, Li$_2$SiO$_3$ becomes the stable phase due to free energy considerations, and a sudden weight loss owing to the full release of CO$_2$ resulted in both samples, as shown in Fig. 4.

Fig. 5 shows the XRD patterns of SG-Li$_4$SiO$_4$ samples before and after CO$_2$ absorption. The virgin samples predominantly contained Li$_4$SiO$_4$ phase, and the samples after CO$_2$ absorption contained lithium metasilicate and Li$_2$CO$_3$ phases. This XRD
3.3. Kinetic analysis of Li$_4$SiO$_4$ absorbent performance

CO$_2$ absorption–desorption profile of materials synthesized from the sol–gel route (SG-Li$_4$SiO$_4$) and solid-state method (SS-Li$_4$SiO$_4$) corresponding to different temperatures are shown in Fig. 6. As the dynamic absorption studies have shown that the absorption rate increased significantly above 500 °C, we have studied the kinetics of CO$_2$ absorption at temperatures above 500 °C in detail. In this study, samples were heated to the absorption temperature at 10 °C min and held for 20 minutes under 100% CO$_2$ gas flow to collect absorption data. Desorption was carried out at 750 °C under the flow of N$_2$ gas. Sample then was cooled to the subsequent absorption temperature. Absorption and desorption rates (calculated from the first 10 minutes) measured at the different temperatures studied are shown in Fig. 7. The maximum absorption rate was obtained at 700 °C and was found to be 22.5 mg g$^{-1}$ min$^{-1}$ for SG-Li$_4$SiO$_4$ and 13.2 mg g$^{-1}$ min$^{-1}$ for SS-Li$_4$SiO$_4$.

Desorption was carried out at 750 °C in all the cases. Desorption rates measured with the sol–gel and solid-state samples were more or less similar; sol–gel samples showed a desorption rate of 25.7 mg g$^{-1}$ min$^{-1}$ whereas the solid-state sample showed a slightly higher value of 26.1 mg g$^{-1}$ min$^{-1}$. Desorption values normally have less dependence on powder uniformity, as the shell of carbonate will be available around all the particles at the instant of the reverse reaction. However, during CO$_2$ up-take the structure of lithium silicate aggregates could determine the overall rate of the process. Comparison of data shown in Fig. 6 and 7 clearly indicates that the samples prepared by the sol–gel route are superior in terms of absorption capacity as well as kinetics. Furthermore, the absorption rate values are comparable to the values reported in recent literature. 29

To clearly understand the rate-determining steps during the absorption process, kinetic calculations were performed on the absorption isotherms of the sol–gel samples by fitting the curves with a double exponential model as reported by other authors. 28 The isotherm was fitted with

$$Y = A \exp^{-k_1x} + B \exp^{-k_2x} + C$$  

In the above equation, $Y$ represents the amount of CO$_2$ absorbed at time $x$, $k_1$ and $k_2$ are the exponential constants for

Fig. 4 Dynamic thermogravimetric analysis of Li$_4$SiO$_4$ samples measured at 20 °C min$^{-1}$ (100% CO$_2$) with respect to temperature.

Fig. 5 XRD patterns of Li$_4$SiO$_4$ (B) and the carbon dioxide-absorbed sample (A). [Li$_4$SiO$_4$ (JCPDS 37-1472), Li$_2$SiO$_3$ (JCPDS 29-0828), Li$_2$CO$_3$ (JCPDS 554-13-2)].

Fig. 6 CO$_2$ absorption kinetic analysis of lithium silicate synthesized by sol–gel method and solid-state reaction.

Fig. 7 Absorption rates of Li$_4$SiO$_4$ at different temperatures (rate values calculated from the first 10 minutes of absorption curve).
the absorption of CO₂ on the surface of the particles and the part of absorption kinetically controlled by the diffusion processes on the bulk, respectively. The \( k_1 \) and \( k_2 \) values calculated for the sample are listed in Table 1. Extremely good fitting could be obtained for all the isotherms, as revealed by the very high \( R^2 \) values in the table. The reported values of \( k_1 \) are usually 10 times higher than that of \( k_2 \), and the same trend could be observed in the data in Table 1 as well. However, there were some deviations in \( k_1 \) and \( k_2 \) values with respect to change in temperature, which could either be due to the nature of the measurement (we have used a continuous measurement mode in our study as in Fig. 6) or the fact that the isotherms were incomplete in our study, as absorption was limited to 20 minutes.

The kinetic constants were fitted against temperature in the range 500–650 °C, where most of the published data are available, and are shown as Arrhenius plots in Fig. 8. The activation energy values for the sol–gel samples were calculated as 70 kJ mol⁻¹ for the chemisorption of CO₂ on Li₄SiO₄ and 37 kJ mol⁻¹ for the diffusion of ions. These calculated values are in line with other published reports, and the higher activation energy values for chemisorption are representative of the absorption of CO₂ on Li₄SiO₄.

### 3.4. Cyclic absorption–desorption performance

The stability and regenerability of synthesized Li₄SiO₄ powders were investigated using cyclic absorption–desorption study at a fixed temperature by switching between 100% CO₂ and 100% N₂ gases. Measurement was performed at the maximum absorption temperature of 700 °C in order to accelerate decay due to any durability issues. The cyclic CO₂ absorption capacities for five consecutive cycles are shown in Fig. 9. Absorption was run at a CO₂ flow rate of 50 ml min⁻¹ and desorption at a N₂ flow rate of 50 ml min⁻¹. The switching was done manually; therefore, absorption–desorption durations have slight variations between cycles. The purpose of the experiment was to see if absorption capacity decreased with cyclic loading due to material loss or segregation. More or less complete CO₂ absorption and release could be achieved in the measured 5 cycles, indicating the structural stability of the materials. However, further studies in 1000’s of cycles are necessary for confirmation of this material’s usage in any commercial CO₂ separation application.

SEM, TEM and XRD studies were performed on the samples after cyclic study (five cycles as in Fig. 9) to understand any variations in morphology or crystal structure that might have occurred to the sample. The electron micrographs as shown in Fig. 10(a) and (b) did not, however, show any significant variation compared to the original samples (Fig. 2 and 3). Powder particles retained their size and morphology to a reasonable extent, although minor changes are visible.

XRD pattern of the samples as in Fig. 11 also well resembled the pattern measured for the original sample (Fig. 5b). Nevertheless, peaks corresponding to the [200] plane were found stronger in the samples after cyclic loading. It is clear that minor changes in crystal structure, and probably morphology, are happening in the sample during cyclic absorption and desorption. However, the changes have not been significant to

<table>
<thead>
<tr>
<th>Temperature (°C)</th>
<th>( k_1 ) (s⁻¹)</th>
<th>( k_2 ) (s⁻¹)</th>
<th>( R^2 )</th>
</tr>
</thead>
<tbody>
<tr>
<td>500</td>
<td>0.0043</td>
<td>0.0004</td>
<td>0.9987</td>
</tr>
<tr>
<td>550</td>
<td>0.0076</td>
<td>0.0005</td>
<td>0.9997</td>
</tr>
<tr>
<td>600</td>
<td>0.0007</td>
<td>0.0190</td>
<td>0.9997</td>
</tr>
<tr>
<td>650</td>
<td>0.0420</td>
<td>0.0010</td>
<td>0.9610</td>
</tr>
</tbody>
</table>

![Fig. 8](image_url) Plots of ln \( k \) versus 1/\( T \) for the two different processes, chemisorption \( (k_1) \) and diffusion \( (k_2) \), observed on the SG sample (a and b).

![Fig. 9](image_url) Absorption–desorption performance of Li₄SiO₄-based sorbent synthesized by sol–gel route (5 cycles at 700 °C).

![Fig. 10](image_url) (a) TEM (b) SEM images of Li₄SiO₄ after 5 cycles of absorption and desorption study.
influence the absorption performance of the samples, at least through the five cycles we have followed in this study.

3.5. CO₂ absorption studies of Li₄SiO₄ coated over porous carbon mesh

One of the main hurdles that limit the practical application of these kinds of absorbents is the difficulty in processing absorbent pellets for large-scale applications. Water-based ceramic extrusion processes have severe hurdles due to the corrosive nature of excess carbonates when dissolved in water. The near-melt condition of the carbonate shell under the absorption-desorption conditions also could give rise to gravity-driven shape deformation of the pellets with time. This could give rise to bulk flow limitations of gases within the absorption column. Supported structures coated in mechanically strong shapes are one way to limit shape deformation. Slurry coating on the support substrate also is easier in terms of fabrication and handling, as issues regarding the corrosive nature of the slurry could be better managed in any dip coating process. Hence, we tried to coat the sol-gel based powders on porous carbon sheets and tested the absorption behaviour of the resulting supported structures.

The surface microstructures of the uncoated and coated carbon sheets are shown in Fig. 12 (a) and (b). The slurry for dip coating was made by ball milling the sol-gel powder in isopropyl alcohol for 72 hours. From Fig. 10(b), it is clear that the coating is uniform over the surface of the form. The absorbent powder weight was ~70% of the total weight of the coated structure.

Cyclic absorption and desorption of the supported sample was carried out at 700 °C using 100% CO₂ and N₂ gases, and the results are shown in Fig. 13. The absorption capacity was 150 mg g⁻¹ for the coated sample (120 mg g⁻¹ within the first 20 minutes as shown in Fig. 13), and the first 60% of absorption was completed at a rate of 37.5 mg g⁻¹ min⁻¹. The measured absorption rate was considerably higher than the value of 22.5 mg g⁻¹ min⁻¹ measured for the powder samples. These results highlight the importance of macrostructure of the powders on the absorption rate. Powder samples normally shape themselves into lump form during the pre-heating stage carried out at 800 °C before the actual absorption measurements, thereby restricting the bulk CO₂ gas flow through them. Coated samples, on the other hand, are capable of keeping the macrostructure intact and therefore could realise superior absorption rates during measurement. In addition, absorption capacity and rate of the coated sample remained same all through the eight cycles measured in our study. It is clear that samples with excellent absorption rates and cyclic stability could be obtained by this fabrication method. The durability of the carbon substrate for long-term use needs detailed verification and is in progress now. Further improvements, in terms of powder loading on the carbon substrates and therefore on the absorption capacity of the coated materials, are also necessary for making the samples useful for any practical applications.

4. Conclusion

Li₄SiO₄ sorbents for carbon dioxide absorption at elevated temperature were synthesized via sol-gel as well as solid-state method. Based on phase evolution studies as well as microstructural characteristics, we concluded that the material developed by sol-gel technique is superior. CO₂ uptake and release studies performed on the samples clearly supported this; sol-gel samples showed an absorption capacity value of
350 mg g⁻¹ and absorption rate of 22.5 mg g⁻¹ min⁻¹. This absorption rate was considerably higher than the corresponding value of 13.2 mg g⁻¹ min⁻¹ measured on the solid-state sample and should be due to the unique platelet morphology of the sol-gel samples. Absorption-desorption cyclic loading studies have shown that the sample remained durable for the five cycles studied. Supported absorbents on carbon mesh were developed, and absorption rates as high as 37.5 mg g⁻¹ min⁻¹ were measured; the samples also showed excellent durability for the 8 cycles measured. Further improvements in terms of powder loading in the supports, leading to higher absorption capacity of the supported structure, may be required for making these supported structures candidates for any practical application.

Acknowledgements

The authors acknowledge the Council of Scientific and Industrial Research (CSIR), New Delhi, India, & Noritake Co. Limited, Aichi, Japan, for providing research facilities and financial support.

Notes and references